Ocean REFuel Stakeholder Meeting - Agenda

- 09:30 10:00 Registration, refreshments
- 10:00 10:15 Ocean REFuel intro/overview
- 10:15 10:30 Work Stream 1 Update (Offshore structures, logistics and power generation)
- 10:30 10:45 Work Stream 2 Update (Power to Carbon Free Fuel)
- 10:45 11:05 Q&A/Discussion/Feedback
- **11:05 11:20** Work Stream 3 Update (Carbon Free Fuel Transportation & Storage)
- 11:20 11:35 Work Stream 4 Update (Networks, Capability and Demand)
- 11:35 11:50 Comfort/Coffee break
- 11:50 12:05 Work Stream 5 Update (Policy framework/Economic modelling)
- 12:05 13:00 Q&A/Discussion/Feedback
- 13:00 Close
- 13:00 13:30 Lunch
- 13:30 ?? Nottingham University Facilities tour (TBC)







Ocean REFuel Workstream 1 Offshore structures, logistics, and power generation

www.strath.ac.uk/engineering

 \times

Workstream 1: the team

Prof Feargal Brennan, Pl







Dr Claudio Rodriguez-Castillo, Postdoc res.



Dr Baran Yeter, Postdoc res. Dr Shen Li, Postdoc res.



Introduction to Workstream 1





Recap of previous results

- NE8 as location: metocean conditions obtained
- Floating offshore wind barge/semisubmersible type most suitable for H2 offshore production



Sconarios >	Basalina	Enhanced LCoE &	Enhanced Deck &	Enhanced Sea- &
Scenarios ->	Dasenne	Resource Potential	Storage Availability	Station- keeping
Alternatives ↓		Closeness to ideal po	ositive solution (1.00)	
Wave-OB (PA)	0.31	0.36	0.23	0.25
Wave-OB (ATE)	0.49	0.47	0.55	0.48
Wave-OWC	0.59	0.54	0.62	0.69
Wave-OVT	0.36	0.38	0.41	0.33
Marine current	0.37	0.36	0.27	0.29
Tidal stream	0.34	0.35	0.25	0.27
Salinity gradient	0.60	0.51	0.66	0.68
OTEC	0.72	0.64	0.79	0.78
Offshore solar	0.41	0.38	0.38	0.37
OWT-fixed monopile	0.63	0.71	0.52	0.71
OWT-spar	0.65	0.71	0.59	0.73
OWT-semi	0.73	0.76	0.75	0.78
OWT-barge	0.75	0.77	0.82	0.76
OWT-TLP	0.67	0.69	0.71	0.74

Platform design and dynamics *Knowledge gaps*

Area ->	Platform design / dynamics	Example
Gaps	 NEW objective / constraints for H₂-producing floating offshore wind turbines? Innovative approach to design/analysis, leading to NOVEL configurations MDAO: Multidisciplinary Design and Analysis approach 	 1.1 Current practice optimising LCoE may not apply → LCoH-optimised design analyses needed (lower power, more stable) 1.2 Platforms fully dedicated to H₂ production better than those using only surplus electricity. NO power connection?
	2. What is the impact of offshore conditions on H ₂ production? H2 Storage?	 2.1 Impact of inclination / velocity / accelerations imposed by the platform on the electrolyser / desalination plant? 2.2 Impact of oscillating power input on electrolyser / desalination plant

Platform design and dynamics *Plan*



Platform design and dynamics *Progress*

N.B. Only an illustrative example, will change shape/dimension



Definition of NOVEL, SPECIFIC critical objectives/constraints

Based on literature and feedback from industry

"Illustrative example" platform numerical model, in realistic metocean

Allow quantification of critical obj/const

Parametric design, allow optimisation



Summary of Platform's weights

	mass [t]	[%]	LCG [m]	TCG [m]	VCG [m]
Total	20679.08	100%	-0.001	0.000	-2.040
Hull struct	3914.00	19%	0.000	0.000	-4.467
Solid ballast	2540.00	12%	0.000	0.000	-18.614
Liquid ballast	11300.00	55%	-0.002	0.000	-16.956
Tower	1263.00	6%	0.000	0.000	56.528
RNA	1016.64	5%	0.000	0.000	149.327
Others (mooring, etc.)	645 44	3%	0.000	0.000	-14 000

Summary of internal volume capacities

	Volume [m ³]	%
Total	26308.12	100%

Pontoons LB	12848.55	49%
Pontoon SB	1257.59	5%
External columns	10060.69	38%
Central column	2141.29	8%

Platform design and dynamics *Progress*



Structures and materials *Knowledge gaps*

Area ->	Structures and materials	Example
Gaps	 New circumstances compromising structural integrity Failure mode, effect and criticality analysis (FMECA) based on multi- stakeholder approach 	1.1 FMECA should involve experts from throughout the whole life cycle to avoid costly design modifications.1.2 Fuzzy-Multi-criteria decision-making seems a promising solution to account for uncertainties regarding the expert opinion.
	 Structural design of semi- submersible structure is unknown. Especially the column where the buffer hydrogen storage will be placed. 	2.1 Design load cases should be investigated for fatigue and ultimate load limit states for the new Floating SS.2.2 How can the hydrogen storage and the protection affect the columns design? - Stored hydrogen is a direct variable for column scantling.
	3. Damage tolerant design is very new to offshore wind; however, there is massive opportunity due to having a FOWT (we can tow it back when needed) and digitalisation	 3.1 Risk-based life cycle management (design, inspection, maintenance, and end-of-life strategies)? 3.2 Adaptive control to mitigate damage and maximise lifetime energy yield? 3.3 Certify structural design through digital twinning – smart certification?

Structures and materials *Plan*



Structures and materials *Progress*



Risk identification & prioritisation

Primary failure causes identified, secondary failure causes to be investigated (HSE consideration)





Years

Structural design

Fatigue design of

welded

connections

Coupling with MDAO Non-standard details?

Structures and materials *Progress*

Digital twinning (Model updating)

Updating digital model using monitored data to minimise modelling discrepancy



Digital twinning (Real-time simulation)

Extrapolate monitored response to enable virtual monitoring of critical yet inaccessible structural details in (near) real time

Motion Strain sensor gauge Sensitivity-based natural frequency model updating **Real-time** $Error = ||\omega - \omega_{DT}||_{e}$ strain/stress, motion etc. Comparison between real and virtual **Design certified?** responses Inspection & maintenance required?

Conclusions

- WS1.1 completed, working on WS1.2, WS1.3
- Main knowledge gaps in *platform design and dynamics* and in *structures and materials* identified
- Plan for gaps: novel platform for novel purpose, therefore:
- Redefinition of objectives and constraints for the overall design (from wind turbine side)
- Modelling to quantify impact of A) motion B) power fluctuation on H2 production and storage equipment (payload side)
- Reassessment of the risks (risk identification and prioritization)
- Novel approaches in structural design damage-tolerant structure and risk-based SI mgmt.
- Digital twinning

University of Strathclyde Engineering



Ocean-REFuel (Ocean Renewable Energy Fuel)

Workstream2: Power to carbon free fuel

Mohamed Mamlouk School of Engineering, Newcastle University 29th March 2023, Nottingham University



Imperial College London











Overview

- 1. Overarching questions of Workstream 2
- 2. Literature Review
- 3. Modelling membrane-less electrolyser results
- 4. Catalyst for AEM based Electrolysers results
- 5. Questions and open discussion





1. Overarching questions of Workstream 2

- 2. Literature Review
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Introduction to WS2

- Can seawater be used directly for efficient production of hydrogen or can seawater purifications be performed effectively offshore producing electrochemically chemicals for water treatment?
- 2. Which electrolyser technology and conditions are most suited to meet performance, cost and hydrogen purity requirements for offshore storage and hydrogen pumping?
- 3. Can electrolysers operate effectively and safely on offshore moored and floating platforms?
- 4. Can offshore electrolyser technology deliver stack performance target <48 kWh/kg (82% electrical efficiency) and costs of system < £800/kW?</p>





1. Overarching questions of Workstream 2

2. Literature Review

Modelling membrane-less electrolyser results
 Catalyst for AEM based Electrolysers results
 Questions and open discussion



Review articles submission

• 1- Review of next generation hydrogen production from offshore wind using water electrolysis





2-Offshore green hydrogen production and

storage







AVVE Advantage and limitations



- Advantage:
- Cheaper CAPEX than PEM, doesn't use precious metal.
- Limitations:
- Bulkier, Poor chemical separation/low H2 pressure, slow system response time, high minimum load

ASR	250 - 350 mΩ cm²
Foot print	20MW 70-150 m2 MW ⁻¹ 1GW 0.1 - 0.17 km ² GW ⁻¹

Nominal current density	0.15-0.7 A/cm2
Operating temperature	70-90C
Lifetime system with stack replacement	20-30 years
Lifetime stack	60,000-90,000h
Electrode area	1-3 m2
Stack capacity	1-2 MW
Capital cost system for 10MW system	\$500-1000/kW
Produced H2 pressure	<30 barg
System energy requirement	54 (50- 78) kWh/Kg H2
Water feed	Ultra pure DI- water 18 MΩ/cm
Cold start to minimum load	20 mins
Ramp up 20-100%	8s (10% /s)
Load range of full capacity	15-100%

PEMWE Advantage and



limitations

- Advantage:
- More compact, higher H2 pressure, faster system response.
- Limitations:
- Require precious metal (e.g. Ir and Pt), more expensive, operate at lower efficiency than alkaline system. Current IrO₂ mining capacity support only
 ASR 50 - 120 mΩ cm²
 Foot print 20MW 35-50 m² MW⁻¹

1GW 0.08 - 0.13 km² GW⁻¹

Nominal current density	1-3 A/cm2
Operating temperature	50-80C
Lifetime system with stack replacement	10-30 years
Lifetime stack	20,000-70,000h
Electrode area	1.5 m2
Stack capacity	2 to 5 MW
Capital cost system for 10MW system	\$700-1400/kW
Produced H2 pressure	20-70 barg
System energy requirement	57 (50- 83) kWh/Kg H2
Water feed	Ultra pure DI- water 18 MΩ/cm
Cold start to minimum load	5 mins
Ramp up 20-100%	2s (40% /s)
Load range of full capacity	5-120%

AEMWE Advantage and



limitations

- Advantage:
- More compact, higher H2 pressure, faster system response than alkaline.
- Limitations:
- Poor stability of membrane separator, poor stability of non precious metal catalyst

ASR 100 - 200 mΩ cm²



Nominal current density	0.2-1 A/cm2
Operating temperature	40-60C
Lifetime system with stack replacement	4 years
Lifetime stack	5,000-10,000h
Electrode area	0.3 m2
Stack capacity	2.5 kW
Capital cost system for 10MW system	n/a
Produced H2 pressure	20-30 barg
System energy requirement	59 (54- 69) kWh/Kg H2
Water feed	Ultra pure DI- water 18 MΩ/cm
Cold start to minimum load	5-10 mins
Ramp up 20-100%	2-4s
Load range of full capacity	5-100%



Membrane-less design

- Advantage:
- Cheaper system due to elimination of membrane cost.
- Can operate with KOH or NaCl electrolyte.
- Limitations:
- Not mature technology. Requires laminar flow, bulkier, lower hydrogen purity, lower current density, balancing flow distribution in electrodes.





To purify or to directly electrolyse sea water? **Energetics**

Challenges

- Chlorine evolution reaction
- pH gradient (energy loss and precipitation)
- Electrode low stability and activity in corrosive Clcontaining electrolyte
- ASR > 0.25 ohm cm² (sea water 30-60 mS cm⁻¹)
- AEM with Cl- ions 2.61 slower than OH⁻
- Concentrated NaCl?

- H2 HHV 39.4 kWh kg_{H2}⁻¹
- Electrolysis 48-54 kWh kg_{H2}⁻¹
- Multistage flash evaporators (MSFE) ullet24-240 Wh L⁻¹ (H₂O) or 0.215-2.15 kWh kg_{H2}⁻¹
- RO 4.2 Wh L^{-1} (H₂O) from sea water or 0.038 kWh kg_{H2}^{-1}
- IEC 0.28 Wh L^{-1} (H₂O)

15 MW electrolyser needs 5.4 m³ h⁻¹ Lenntech 10 m³ h⁻¹ 11kW (low saline) RO plant footprint 3.5 m² Wartsila 10 m³ h⁻¹ 1.85MW MSFE footprint 20 m², 32 ton





Overarching questions of Workstream 2 Literature Review Modelling membrane-less electrolyser results Catalyst for AEM based Electrolysers results Questions and open discussion

Porous Microstructure generators



Porous Microstructure Generator (PMG)

Porous Microstructure Generator



Download all (166.7 MB) Share Embed + Collect

Version 4 🗸	Software posted on 2022-12-09, 10:57 authored by Daniel Niblett,	
Mohamed Ma	mlouk, Omar Emmanuel Godinez Brizuela	

Porous Microstructure Generator (PMG) is a GUI software that can generate computational 3D structures of porous materials using a set of customised algorithms. The surfaces can be exported as .tiff or .stl for use in other simulation software.









Daniel Niblett



Wewcastle University

Programme development for cell model creation





Dynamic 2D 2phase simulations



A/cm2 for case 1 and case 2.









0-84kA/m²

0-100kA/m²



6.0e-03

0.005

0.004

0.003

- 0.002

0.001

0.0e+00

3.1e-01

- 0.25 - 0.2 - 0.15

0.1

- 0.05 0.0e+00

Velocity distribution (1phase)



Dissolved gas crossover



Dissolved H2 concentration with Reynolds number





Video @ 1 A/cm2. 10 cm geometry.

H2 concentration in O2 stream



- Safety
- Gases purity
- Minimum load and dynamics





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Ni based LDH electrode for OER



Shanmugam









Direct growth of Layered double hydroxide on Ni Foam by using hydrothermal method

Morphology analysis : (a-e) SEM images of LDH @ Ni foam with different magnifications


MOx on LDH electrode for OER









Growth of metal oxide on LDH / Ni foam by using hydrothermal method

Morphology analysis : (a-d) SEM images of metal oxide /LDH @ Ni foam with different magnifications

Electrochemical performance AEM electrolyzer (1)





Electrochemical performance AEM electrolyzer (2)









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Questions and discussion

Ocean Refuel funded by EP/W005204/1





Ocean-Refuel

Work Stream 3: Transportation and Storage

WP3.1 Solid State Hydrogen WP3.2 Ammonia as a Hydrogen-Rich Carrier















Work Package 3.1 Solid State Hydrogen storage and compression

Marcus Adams, Amelia-Rose Edgley Alastair Stuart, David Grant, Gavin Walker

Faculty of Engineering | Faculty of Science | Faculty of Social Sciences





Work Packages



- WP3.1.1: Impact of impurities from a range of cost-effective electrolysers
- WP3.1.2: Metal Hydride Hydrogen Buffer Store
- WP3.1.3: Metal hydride compressors as an efficient, non-mechanical compression system

WP3.1.4: Fuel transportation to other regions (HT or LT MHx)





WP3.1.1: Impact of impurities from a range of cost-effective electrolysers



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Nanostructured hydrogen materials for offshore green hydrogen **Amelia-Rose Edgley**

Compressor

Aims

- Create higher capacity • metal hydride stores
- Improved tolerance to impurities

Materials challenge

- Low temperature for • hydriding/dehydriding
- Maintain good volumetric • capacities
- **Retain good kinetics** •





Wind Turbine





Metal Hydride **Buffer Store**



Salt Cavern Store





Electrolyser





WP3.1.2: Metal Hydride Hydrogen Buffer Store



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Hydrogen R



MH Buffer Store Test Facility



- Hardware in the Loop test facility
- 100 bar max pressure
- Test stores up to 1 kg hydrogen

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Simulato		C
Simulate		N
Electrolyser		S
		-

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Ocean Refuel Metal Hydride Store Simulate controlled hydrogen delivery





 Manually crushed 1.6 kg of solid-state H₂ alloy

MH Store small scale store

To test activation method at larger scale

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Nottingham









WP3.1.3: Metal hydride compressors





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MH Compressors - explained

- MH Compressors are driven by heat, not electricity.
- Electrolyser waste heat can be used to compress hydrogen.
- The minimum energy requirement for a single stage is ≈ 4 kWh/kg H₂
- (1 2) Hydrogenation
- (2 3) Bed heating

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- (3 4) Dehydrogenation
- (4 1) Bed cooling
- A 2nd stage can be added if a higher pressure is needed.



Hydrogen capacity of MH







- Electrolyser waste heat can be used to compress hydrogen.
- The minimum energy requirement for a single stage is ≈ 4 kWh/kg H₂
- Example electrolyser (Enapter):

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- Electrical consumption 53.3 kWh/kg(H₂)
- Waste heat = 13.9 kWh/kg(H₂)
 - o based on HHV



www.enapter.com/newsroom/kb_post/what-is-the-overall-efficiency-of-enapters-electrolyser



Aim: Compress from 30 bar to 100 bar using only waste heat from an electrolyser.

Hydrogenate @ 5 – 15 °C. Dehydrogenate @ 80 °C



Material challenge: Reduce the slope for the plateau to make each stage more efficient.

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Commissioning MH Compressor





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- Commissioning a 2-stage MH compressor test facility.
- Intend to use a lattice structure for improved heat transfer.
- Initial plan to optimise materials and test effectiveness of these materials to compress from 30 bar to 100 bar.
- Based on AB2 compositions



Ocean-Refuel





Engineering and Physical Sciences Research Council

Any questions?



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@UoNEnergy



WP4 -Networks, Compatibility and Demand

H2 may be transported in its pure form, transformed into a different energy carrier and/or blended to form part of a gas stream to be transported. Ammonia can support the concept, whilst methane produced from capture CO2 and H2 could mitigate the impact of excessive carbon dioxide emissions.

The WP addresses,

WP4.1. Use of NH3 as an alternative long-term/long-distance energy vector

WP4.2. 'Carboniferous' Hydrogen Supply

WP4.3. Public Perception of technologies

WP4.4. LCA and System Metrics

WP4.5. Overall System Optimisation



4.1. Use of NH3 as an alternative long-term/long-distance energy vector

Task 4.1.1. Numerical and experimental data on efficiency, energy, costs for LCA a nd system studies.

Task 4.1.2. Integration of systems for higher efficiencies to various sectors.

Task 4.1.3: Study for the reconversion of ammonia to hydrogen at a larger "city-gate" scale.

WP4.1. Ammonia application prospect

CARDIFF UNIVERSITY PRIFYSGOL CAERDYD



- Ammonia has a high energy density and can be used as a fuel in combustion engines, gas turbines, and fuel cells.
- Ammonia is a promising energy carrier for renewable energy sources.
- Ammonia is a cost-effective alternative to conventional fuels, such as gasoline and diesel, particularly in regions with high renewable energy potential.





Overview









- Ammonia storage;
- Ammonia distribution;
- Ammonia combustion;
- Ammonia cracking;
- H2 boiler;
- Storage of heat from renewable and sustainable energy source;
- Long-distance of ammonia transportation;
- In-real time household heating.

Dual heat source ammonia-based heat pump system





30/03/2023

Temperature variations





- Room temperature can be maintained at a desired set point under various weather conditions.
- Initial flow rate control and heat source switch may cause minor temperature fluctuations.
- Soil and grout temperature may gradually decrease during winter.

IC Engine (Experimental Component)







- ICE Purchased and promised by October 2022. However, supplier issues (caused by the war), staff problems and other inconvenients have delayed the delivery of the unit.
- Latest run (15 March 2023) showed that the engine is still suffering from poor ignition (?).
- The company is bringing specialists from Denmark and Germany to support them and deliver ASAP.

UK SCENARIO FOR AMMONIA UTILIZATION





Unfortunately, Orkney project has been cancelled. ENEUS is providing us information for the analysis of the ammonia plant based on a project they are commissioning in the US.



4.2'Carboniferous' Hydrogen Supply

4.2.1 Safety Assessment

4.2.2 End-use performance

(4.2.3 Accurate Flow metering)





What on earth is 'Carboniferous' H_2 ?

- Two operational scenarios
- Early operation limited hydrogen availability H₂ blended into NG systems
- 2. Late operation systems incapable of retrofit with pure H_2 supplied by a blend of H_2 and CH_4 synthesised from H_2 and captured CO_2 .

Need to understand the capabilities – and operational range – of components that may need to operate on a range of gas compositions during their useful lives.



4.2.1 Safety Assessment

- Design and procurement of new test equipment to domestic-scale appliances at blends from 0-100% H₂ in CH₄
- Conversion of lab-space to put in place safety improvements to enable H₂ use – extraction, flashback protection, gas detection and safety interlock systems
- Imminent system installation and commissioning
- 'Learning by doing' our own safety considerations inform the wider safety debate





4.2.2 End-use performance

- Acquisition of 'commercial' burners designed for 50% $\rm H_2$ optimal operation and 100% $\rm H_2$ optimal operation
- Both burners to be tested at, and away from, nominal design conditions (blends)
- Emissions, stability, appearance and other operational parameters to be assessed.
- Review of literature complete data for up to 30 (mol) arrestor
 % H₂ and 'pure' H₂ but little in between.
- Active interaction with regulators to understand what likely future performance targets may be.







WP4.3. Public Perception of technologies

Task 4.3.1 Assessment of publics' perceptions

- Dr Christina Demski moved from Cardiff University to Bath University, taking this task with her.
- Bath and Cardiff are finishing the signature of an agreement to work on the project. As soon as the final signature is agreed (exp. April 2023), Bath will start the recruitment process of an RA to start with the Public Perception analysis.





4.4 LCA and system metrics

- Recruitment for PDRA post in contract stage
- Initial literature survey and analysis completed by PGR researchers with focus on:
- 1) Resource requirements of PEM electrolysers and potential for circular management
- 2) Wind turbine technology types and associated material requirements




Comfort Break







Ocean-REFuel (Ocean Renewable Energy Fuel)

Cross-cutting: systems engineering

WPS4



Systems engineering questions



- Where to establish the system boundary (especially on the demand side)
 - How far onshore to explore infrastructure (in conjunction with WP4)
- Where will our fuels be most valuable?
- How does that compare with the most favourable supply location?
- Are there opportunity costs in the conversion process (displacement of useful renewable electricity)?
- What vectors are best to move between locations (electricity, H2, chemical fuels, ...)?
- How to operate the system dynamically?
- How does the system dovetail with the UK's energy (and hydrogen strategy) to 2030 and beyond?
- Where are the innovation and policy pinch-points in the system?



Context: Hydrogen – roles in the future energy system

- Industrial feedstock and reductant
 - Existing and new processes (iron, synthetic fuels, ...)
- Industrial, commercial and residential heating
- Low carbon power generation/CHP
- Transport
 - Heavier duty/longer range vehicles, trains, marine, aviation?
- Energy storage and renewables integration/cost reduction
- Long distance low-carbon energy transport

Systems engineering: aim to establish how "best" the system evolves over time



Context: UK H2 roadmap



System design: problem statement



- 1. location of offshore wind farms,
- 2. Technology selection
 - 2.1. Electrolyser type : turbine-integrated, wind farm hub, alkaline, PEM, or SOEC
 - (centralised or decentralised)
 - 2.2. Energy transmission method: direct through cable , indirect through hydrogen carrier (hydrogen, ammonia, etc)
 - 2.3 Desalination technology
- 3. Dynamic operation and control
- 4. Integration with onshore infrastructure what is required at port-side and what is assumed beyond?

What are the metrics to assess the system (e.g. system value, levelised cost of energy,)? How to ensure effective integration (not competition) with onshore fuel production?

Ongoing research: System optimisation problem formulation

Objective function: levelized costs of fuel
Constraints: Satisfying demand for electricity and hydrogen over the time horizon
Constraints: modelling economics, including capital costs and operational expenses,
Constraints: energy balance of electricity flows,

Constraints: mass balance of hydrogen flows,

- Constraints: lean model (perform. curves) of electrolysers,
- Constraints: lean model (perform. curves) of fuel cells,
- Constraints: Electricity network model

Constraints: technical limitation of process equipment, and infrastructure

Integration with LCA and wider environmental analysis (UNott)

Exploration of different on- and off-shore storage options (UNott)



Source: ArcGIS – UK Offshore Wind Energy (Link)

Data requirements

- The location of existing offshore wind farms,
- The potential location of future offshore wind farms,
- The wind profile associated with the location of existing and potential wind farms
- The potential of integrating electrolyser with future WTs, and possible architectures
- The temporal distribution of demand for hydrogen and electricity over 2023-2030 time horizon
- The (offshore) performance of the electrolyser technologies [PEM, AWE, SOEC,]



Previous related research: Integrated design and operation of 1GW facility



System dynamics





Current analysis: trade-offs



- Pathway 1: floating wind array, offshore electrical substation, HV export to onshore substation, PEME onshore
- Pathway 2: floating wind array; interarray cables to a centralised PEME electrolysis off-shore platform. Hydrogen gas pipeline to shore.
- Pathway 3 integrated electrolysis at each floating turbine with inter-array hydrogen collectors and hydrogen pipeline to shore.



Parameter variation



Preliminary results: CAPEX and LCOH



Next steps

- Finalise version 1.0 of systems optimisation model
- Locate this in a specific geography based on the "strawman"
- Data integration with other workstreams
- Develop a "base case" design
- Explore sensitivities and identify performance-limiting aspects of the system
- Explore trade-offs....

Ocean REFuel Workstream 5 Policy framework/economic modelling



UNIVERSITY of STRATHCLYDE CENTRE FOR ENERGY POLICY

www.strath.ac.uk/humanities/centreforenergypolicy/

Workstream 5: the team

Professor Karen Turner, WS5 lead



Dr Antonios Katris, CEP Research Associate



Dr Abdoul Karim, postdoc researcher



Hannah Corbett, knowledge exchange fellow







- The wider policy challenge
- Ocean REFuel capability and capacity for policy and economic analyses
- Learning from previous research and energy supply activity
- Policy and research challenges



From our bid, linking to Networks, Capability and Demand

'How will industry, public and regulators/politicians perceive the technology solutions themselves, and the wider economy impacts of developing, deploying, and using the technology? This is crucial in informing policy narratives around which consensus can build.'



Capability and capacity for policy and economic analyses

Expertise in modelling of wider economy implications, consequences, identifying policy trade-offs and considering routes to mitigating less desirable outcomes

- 'WS5' defined across other workstreams, to complement and build on technoeconomic analyses through use of multi-sector economy-wide computable general equilibrium scenario simulation models
- Aim of building understanding of how in terms of how energy supply, storage and transportation solutions emerging may integrate with current energy supply and use sectors and impact across the wider UK economy.
- Use of results to inform policy analyses and narrative development.



Computable general equilibrium (CGE)

- Multiple sectors (industries and consumer) and markets
- 'General equilibrium'
- Options regarding specification at industry/sector and final consumer level, in different markets, and what we assume about government budgetary approach, how labour markets function etc.
- Aim to avoid 'black box'
- Widely used and trusted in research and policy communities









Learning from previous research: e.g., CCS and integrating a new CO_2 transport and storage industry into the economy

- Once operational, CO₂ T&S likely to share supply chain characteristics with existing UK Oil and Gas industry
- Extensive upfront infrastructure investment required
- Competition with other sectors and projects for resources; likely need for government intervention to involve guaranteeing demand for capacity
- Depending on who pays, how and when, has potential to deliver sustained net wider economy expansion with new jobs and GDP creation

February 2023 CEP Policy Brief - https://doi.org/10.17868/strath.00083992





Competition for constrained resources, particularly labour

- Where demand for workers/skills increased and labour supply is constrained, introduces wage cost pressure that benefits workers/households, but pushes up costs in all sectors
- Consequent domestic and international competitiveness challenges and consumer price impacts
- Displacement of employment across multiple sectors (particularly labour-intensive – e.g. services)

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Conceptualising the nature and role of the offshore energy sector

- Effectively a new sector(s) in the economy?
- That is, doesn't yet exist/report in economy-wide national accounts (input-output, IO, tables reported by ONS)
- Can we identify benchmarks/proxies from current IO?
 - Electricity, transmission and distribution?
 - Gas; distribution of gaseous fuels through mains; steam and air conditioning supply?
- Currently working on breaking out single national accounting 'electricity' sector to identify network, trade, different types of generation and storage potential.
- Enables initial 'what if' reporting and scenario simulation
- Including focus on benefits of retaining already established supply chain capacity and addressing challenges where domestic capacity has not developed (e.g., onshore renewables in Scotland)
- But also need to investigate differences in what is produced, how valued and by whom
- Benchmark basis for consultation to ultimately refine to how new industry activity actually integrates into economy





A wide range of policy and research challenges

- The integration of new energy supply options into the economy is complex
- Once we've established what new energy supply, storage and transportation sectors look like, and what are they producing, just how are they deployed?
 - E.g., is there a need to initially over-size capacity what are the capital expenditure implications, who pays, how and when, how can the process be de-risked?
 - How can competitive domestic supply chain capability and capacity emerge where it has been lacking before (e.g., onshore renewables)?
- What demand do new sectors serve, what and how do they replace and/or integrate with via existing/new networks and markets?
 - E.g., industrial use of hydrogen may begin with continued purchase and 'in-house' reforming of natural gas, which will have (sunk?) investment and network implications for firms – how does hydrogen ultimately become a substitute for industrial users?
- Which actors (industry, regulator, government) are responsible, able and willing to act at what stages in the supply/demand process?
- How can/will the picture evolve over time and under different circumstances?





Questions and discussion

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